



Compliance Monitoring Report

Consent Holder

Affco New Zealand Limited

Consent No DP070026Aa

Client Address

PO Box 243

Site Address

Hunter Brown Street, Wairoa

Wairoa 4160

Phone

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Contact Name

Paul Sullivan

Mobile

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Job Code

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Consent Type

Discharge Permit

Activity Description:

to discharge contaminants into the air from the operation of the company's meat processing operation at Wairoa, including the following processes:

-Products of combustion from a 15 MW coal fired boiler

-Fellmongery

-Effluent treatment plant

-Rendering plant

-General associated operations to those above.

16-Nov-10

Monitoring Report Sent

Officer

Barbara McKenzie

28-Jul-11

Monitoring Inspection

Officer

Jim May

19-Apr-12

Monitoring Inspection

Officer

Jim May

01-May-12

Monitoring Report Sent

Officer

Barbara McKenzie

2011-2012 Statement of Compliance and Overall Grades:

Grade Date

01-May-12

Environmental Grade

Compliance

Technical Grade

Compliance

Overall Comments:

Full compliance with the conditions has been achieved. Conditions 7 and 16 are under review.

Grade Date

02-Jul-12

Environmental Grade

Compliance

Technical Grade

Compliance

Overall Comments:

Full compliance with the conditions has been achieved. Condition 7 will be assessed when Council receives the next stack test report and Condition 16 will need to be changed if fleshings continue to be rendered.

Previous Statement of Compliance and Overall Grades:

Grade Date

11-Nov-10

Environmental Grade

Compliance

Technical Grade

Compliance

Overall Comments:

Full compliance with conditions has now been achieved.

Refer to back page for grading information

Condition No.	Type of Condition	Consent Condition and Compliance Assessment
1	Technical	The consent holder shall undertake all operations in accordance with any drawings, specifications, statements of intent and other information supplied as part of the application for this resource consent. In the event that there is a conflict between the information supplied with the application and any consent condition(s), the conditions(s) shall prevail.
	Compliance	11-Nov-10
	Compliance	01-May-12 Administration.
2	Environmental	The concentration of hydrogen sulphide shall not exceed 7 (g/m3, as a 1 hour average, in the ambient air at or beyond the boundary of the premises as a result of emissions from the consent holder's property.
	Not applicable	11-Nov-10
		Monitoring to this level is not required until the Fellmongery is commissioned. Council has not received any complaints for hydrogen sulphide odours.
	Compliance	01-May-12
		While Council has not tested the ambient air at this site, there have not been any complaints this season for hydrogen sulphide.
3	Environmental	There shall be no discharge of any objectionable particulate matter on any land or structure beyond the boundary of the site.
	Compliance	11-Nov-10
		Council has not received any complaints for particulate discharged. The boiler was not operating during the site inspection.
	Compliance	01-May-12
		The Council Officer did not observe any particulate in the discharge during the site visit and there have not been any complaints.
4	Environmental	There shall be no discharge of offensive or objectionable odours beyond the boundary of the site.
	Compliance	11-Nov-10
		The biosolids bark filter and extraction system have been installed, the shed reclad.
	Compliance	01-May-12
		The Council Officer did not detect any offensive or objectionable odours while on site and there have not been any odour complaints.
	Compliance	02-Jul-12
		The Council Officer did not detect any odours that were either offensive or objectionable while on site 19 June 2012.
5	Environmental	Emissions of combustion products from the coal fired boiler shall be discharged through a chimney not less than 30 m high at a minimum efflux velocity of 10 m/s at full load. The discharge shall be vertically upwards and unimpeded.
	Compliance	11-Nov-10
		Observed to be the case. The boiler was not operating during the site inspection.

Condition No.	Type of Condition	Consent Condition and Compliance Assessment
	Compliance	01-May-12
		The chimney height and discharge velocity have not changed.
6	Environmental	The discharge to air from the coal fired boiler system shall not exceed a PM10 concentration of 200 milligrams per cubic metre of gas (expressed at 0(C and on a dry gas basis, standardised to 12% CO2), before discharging to the atmosphere, prior to 31 December 2010. If emission testing indicates levels in excess of this condition the consent holder shall, within two months, arrange for a repeated emission testing.
	Unable to be ass	sessed 11-Nov-10
		The latest test results have not been submitted yet.
	Compliance	01-May-12
		Council has received the Air Discharge Stack Testing Report. The results confirm compliance with this requirement.
7	Environmental	By 31 December 2011 the discharge to air from the coal fired boiler system shall not exceed a PM10 concentration of 100 milligrams per cubic metre of gas (expressed at 0(C and on a dry gas basis, standardised to 12% CO2) before discharging to the atmosphere. If emission testing indicates levels in excess of this condition the consent holder shall, within two months, arrange for a repeated emission testing.
	Not applicable	11-Nov-10
		This condition applies after 31 December 2011
	Not applicable	01-May-12
		The consent holder has made an application to adjust the timing for this requirement. This condition will be assessed when the changes have been granted.
8	Technical	Emissions of PM10 shall be exempt from Conditions 6 and 7 above, for the 30 minutes following the start up of the boiler from cold, and during soot blowing, provided all practicable measures are taken to minimise the emission of smoke.
	Compliance	11-Nov-10
	Compliance	01-May-12
		Observed to be the case.
9	Technical	By the 30th September 2010, the consent holder shall provide a report to the Council (Manager Consents) showing the options available to achieve compliance with Condition 7, and the preferred option. This may include a schedule for investigating whether NES exceedances are an issue arising from this discharge.
	Compliance	11-Nov-10
		Council received the report 29 September 2010.
	Not applicable	01-May-12
		This condition is now historical.
10	Environmental	If the drying of biosolids occurs, the biosolids drier shall be ventilated to the rendering plant biofilter detailed in Condition 12.

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Condition No.	Type of Condition	Consent Condition and Compliance Assessment						
	Not applicable	11-Nov-10						
		The consent holder is not drying the biosolids.						
	Compliance	01-May-12						
		The foul air from this process is extracted to the biosolids biofilter.						
11	Environmental	The coal fired boiler shall be operated:						
		a) using coal with a sulphur content of not more than 0.5% by weight, and an ash content not more than 5% by weight.						
		b) using biosolids(de-watered sludge), pre-dried to not more than 25% moisture in the coal fired boiler.						
		c) by substituting not more than 20% of the coal fuel with dried biosolids.						
		d) with biosolids sourced from the on-site effluent treatment plant only.						
	Compliance	11-Nov-10						
		Results on site confirm compliance with this condition.						
	Compliance	01-May-12						
		Coal records on site confirm that the sulphur and ash levels in the coal are below the requirements.						
		At present the pre-dried biosolids are not used as a fuel in the boiler. Therefore Condition 11 subsections (b-d) are not applicable.						
12	Environmental	The rendering plant shall at all times, and at all odour sources, be point source ventilated to a bio-filter and the following monitoring and maintenance practices shall take place to ensure that the system continues to effectively contain odour:						
		a) Weekly monitoring and correction of the negative pressure on the suction side of the extraction fan. (Significant changes in this pressure are an indication that the system may require rebalancing, or that a blockage or leak may have developed).						
		b) Daily inspection and correction of the system for water vapour/odour emissions.						
		c) Daily inspection and correction of any raw material and product leaks that develop.						
		Details of all inspections, completed actions and the corrections made, shall be recorded. Records shall be made available to Council Staff on request.						
	Compliance	11-Nov-10						
		Observed to be the case. The plant was not operating during the site inspection.						
	Compliance	01-May-12						
		Both the rendering plant and biosolids biofilters are checked and maintained as required by this condition.						
13	Technical	By 31 May 2009 the consent holder shall submit a report from a suitably qualified person, for approval to the Council (Manager: Regulation), detailing the size and design of the biofilter for the rendering plant required by Condition 12.						

Condition No.	Type of Condition	Consent Condition and Compliance Assessment
	Not applicable	11-Nov-10
		This condition is now historical.
	Not applicable	01-May-12
		This condition is now historical.
14	Environmental	Negative pressure shall be maintained at all times within the rendering plant to minimise fugitive emissions.
	Compliance	11-Nov-10
		Observed to be the case when the plant was operating.
	Compliance	01-May-12
		There is point source extraction from the process.
15	Technical	Prior to construction of the rendering plant commencing, the consent holder shall submit a report and associated plans from a suitably qualified person, for approval to the Council (Manager: Regulation), detailing how the rendering building will be designed to allow subsequent biofilter connection.
	Not applicable	11-Nov-10
		This condition is now historical.
	Not applicable	01-May-12
		This condition is now historical.
16	Environmental	Raw material to be processed in the rendering plant shall be only sourced from the consent holder's premises that are the subject of this consent.
	Compliance	11-Nov-10
		Informed to be the case.
	Compliance	01-May-12
		There is a sanctioned fleshings processing trial at the plant. If the trial is successful economically and environmentally, then the consent holder intends to apply to have this condition altered.
	Compliance	02-Jul-12
		The fleshings trial has been completed. If this activity is to continue, this condition will need to be changed.
17	Technical	Within 16 months of the commencement of consent, if the biosolids belt press is still in operation, the biosolids building shall be fully contained and ventilated to a biofilter.
	Significant Non	Compliance 01-Mar-09
		The biofilter has not been installed by 1 March 2009.
	Compliance	09-Nov-10
		The biosolids building has been reclad and a biofilter and extraction system installed.
	Not applicable	01-May-12
		The biosolids biofilter has been installed.
		This condition is now historical.
18	Technical	Where a biofilter is required in accordance with Condition 17, the consent holder shall submit a report from a suitably qualified person, for approval to

Condition No.	Type of Condition	Consent Condition and Compliance Assessment
		the Council (Manager: Regulation), detailing the size and design of the biofilter for the biosolids building.
	Compliance	11-Nov-10
		Council received this report
	Not applicable	01-May-12
		This condition is now historical.
19	Technical	The consent holder shall undertake emission testing of the coal fired boiler every six months until 2011, and annually thereafter. Emission testing shall be carried out when the coal fired boiler is running on mixed fuel, and when the coal fired boiler is running on coal only. The following test methods shall be used (or equivalent method to the reasonable satisfaction of the Council (Manager: Regulation), to determine the concentration of the following contaminants:
		□ NO2 - Electrochemical or USEPA Method 7
		□ PM10 – USEPA Method 201A
		□ SO2 – Electrochemical or USEPA Method 6
		□ CO – Electrochemical or USEPA Method 3
		The results of these tests, and the ratio of biosolids:coal, shall be forwarded to the Council (Manager: Regulation) within one month of the tests being carried out.
	Compliance	11-Nov-10
		Report received.
	Compliance	01-May-12
		Council has received this report.
		The tests required by this condition are conducted by CRL Energy Ltd.
20	Technical	Annual testing shall be carried out to measure the concentration of hydrogen sulphide in the ambient air beyond the boundary of the premises. These tests shall be carried out by the Council, or by a suitably qualified person using test methods as authorised by the Council (Manager: Regulation). The consent holder shall meet the costs of this monitoring.
		Note: this monitoring will not be carried out until the Fellmongery is commissioned.
	Not applicable	11-Nov-10
		The monitoring required by this condition only applies when the Fellmongery has been commissioned.
	Not applicable	01-May-12
		A fellmongery has not been commissioned yet.
21	Technical	The consent holder shall prepare within 6 months of the commencement of this consent, a management plan that addresses the following:
		 a) Identification of all significant odour sources on site, the procedures in place to address each odour source, and procedures in place for any periods of malfunction.
		b) Operating procedures for the biofilters and any maintenance required to

Condition No.	Type of Condition	Consent Condition and Compliance Assessment
		be undertaken.
		c) The management plan shall require the development of a system which will record details of inspections, measurements and maintenance undertaken on any odour control system, any periods of malfunction, the reasons and the remedial action taken.
		d) The measures in place to ensure isolation and/or segregation of chemicals involved in the Fellmongery process (this part of the management plan is required prior to commissioning of the Fellmongery).
		The management plan and records shall be made available to the Hawke's Bay Regional Council on request.
	Compliance	11-Nov-10
		The consent holder has completed (except part d) the Air management Plan as required.
	Not applicable	01-May-12
		This condition is now historical.
22	Technical	The Consent Holder shall facilitate, in conjunction with the AFFCO Wairoa Odour Working Party, regular meetings at a frequency determined by the consent holder and the AFFCO Wairoa Odour Working Party, but not less than once in each calendar year. Minutes from these meeting shall be made available to the Council on request.
	Compliance	11-Nov-10
		These meetings have been conducted. There appears to be a dwindling number of public attendees.
	Compliance	01-May-12
		The consent holder has facilitated these meetings. The last meeting was poorly attended by the public.
23	Technical	The Consent holder shall record all complaints received. The record shall include:
		a) the date and time of the complaint,
		b) the nature of the complaint,
		c) the name, telephone number, and address of the complainant,
		d) weather information (an estimate of wind speed and direction)
		e) details of key operating parameters at the time of the complaint,
		f) corrective action taken.
		Complaints shall be reported to the Council as soon as practicable and the log of complaints shall be made available to the Council on request.
	Compliance	11-Nov-10
		Complaints have been recorded and reported to Council as required.
	Compliance	01-May-12
		No complaints have been received. However, the consent holder has a system in place to address any complaints received.

Grading Information

Each consent condition has been classified as either a Environmental or Technical condition.

Environmental conditions:

Environmental conditions set standards/performance limits for a resource consent, or, mitigates an environmental impact of exercising a resource consent.

Examples of environmental conditions are:

- Installation of up-gradient cut-off drains/ placement of disposal fields
- volume limits of discharges
- water take rates and maximum volumes
- discharge or receiving water contaminant limits

Technical conditions:

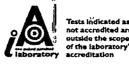
Technical conditions sets out technical requirements that allows a consent holder to demonstrate or measure that they meet the Environmental performance required by a resource consent, or help specify the activity authorised.

Examples of technical conditions are:

- sampling effluent/ recording discharge volumes / collating submitting data
- providing of reports/ plans/ designs specifications
- notifications, accreditation, authorities submissions for approval by ER Manager
- installation and maintenance of a water meter

You need to comply with all conditions regardless of whether it's a Environmental or Technical condition.





Author(s):

CRL Ref: [

Client Name:

Client Address:

Date Of Issue:

Prepared By:

Title:

Consent Number:

PM₁₀ and TOTAL SUSPENDED PARTICULATES (TSP)

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DP070026A

Affco Walroa

P.O.Box 243

5th April 2011

Wairoa

PM₁₀ Particulate Emission Report

John Thompson Boiler

ISO 9001

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Introduction:

CRL Energy Ltd Air Quality Group was commissioned by AFFCO Wairoa to perform particulate testing on the John Thompson boiler. The purpose of the monitoring was to assess compliance of the boiler as per resource consent no \$DP070026A.

The John Thompson boiler tested has been commission by Easteel. The boiler's combustion controls have been fully automated. The plant's emissions exit via one emission source. For emission control the boiler is equipped with twin grits and fly ash hoppers

Maurice Arnott and Steven Gale of the CRL Hamilton branch carried out the tests on the 29th of March 2011.

Test Method:

The method employed was USEPA Method 201A – Determination of PM₁₀ Emissions (Constant Sampling Rate Procedure).

A sample of gas was withdrawn at a constant flow rate from the stack through a size-selected nozzle coupled with a PM_{10} cyclone unit. The PM_{10} cyclone operates by drawing air tangentially into a cylindrical body and causing the particles to be separated in size by centrifugal force. Particulate matter equal to or less than 10μ proceeds through the unit where it is finally collected onto a glass fibre filter, whereas particulate matter greater than 10μ is forced out onto the walls of the cyclone and retained in the cylindrical body. This cyclone unit was kept inside the stack during the test time period. Particulate mass is determined gravimetrically subsequent to the removal of uncombined water.

Determination of a suitable flow rate, nozzle size, and length of sampling was achieved using averaged data obtained from an initial assessment prior to sampling.

Percentage moisture content was also determined. Moisture was condensed and collected into Greenburg-Smith impingers. The impingers were weighed before and after testing.

The PM₁₀ result is expressed as mg/m³ on a dry gas basis and at STP (STP being 1 atm and 0 Deg C) and as a percentage of total particulate collected. The result can be corrected for oxygen or carbon dioxide depending on air discharge resource consent requirements.

Factors That May Influence The Test:

One significant limitation concerning USEPA Method 201A involves the moisture content of the flue gas; the gas cannot contain entrained water droplets. Additionally, an appropriate sampling time should be employed such that a \pm 5% precision on total collected mass as determined by the precision and sensitivity of the measuring technique is achieved. This variable can be problematic on new untested stack emission sources where the technician does not know accurately the typical quantities of particulate emitted. Compounding this problem further is where the particulate concentration of the stationary stack is extremely low, in which case a very long sampling period would be required in order to achieve results with a precision of \pm 5%.

Plant Operating Conditions:

The John Thompson boiler was running on 28mm to 50mm nugget coal, supplied by Solid Energy.

The average steam flow during the first test was approximately 8.5 T/hr and 8.7 T/Hr for the second test and 8.0 T/Hr for the third test.

Further detail is available from in Appendix 3 from the steam flow and O2 chart.

Discussion and Conclusion:

On the 29th of March 2011 the average PM₁₀ concentration of particulate matter from the John Thompson boiler stack was below the Air Discharge Consent limits for 31st of December 2003 but above the new consent limit of 100 mg/m³.

AFFCO Wairoa's Air Discharge Consent states that "The discharge to air from the coal fired boiler system shall not exceed a PM₁₀ concentration of 200 milligrams per cubic metre of gas (expressed at 0°C and on a dry gas basis, standardised to 12 % CO₂) before discharging to the atmosphere, prior to 31 December 2010".

The PM₁₀ concentration obtained for Test 1 was 149 mg/m³ at STP (0°C and 1 atm) and 12% CO₂ and dry gas basis; which is above the new 100 mg/m³ consent limit.

The calculated PM₁₀ concentration obtained for Test 2 was 155 mg/m³ at STP (0°C and 1 atm) and 12% CO₂ and dry gas basis; which is above the new 100 mg/m³ consent limit.

The calculated PM₁₀ concentration obtained for Test 3 was 135 mg/m³ at STP (0°C and 1 atm) and 12% CO₂ and dry gas basis; which is above the new 100 mg/m³ consent limit.

The average PM₁₀ concentration obtained for AFFCO Wairoa's John Thompson boiler stack was 146 mg/m³ at STP (0°C and 1 atm) and 12% CO₂, which is above the new 100 mg/m³ consent limit.

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CRL Reference:	11-31304 Date of Test: 29/3/11	Company	Affco Wairoa	· ·
Description of Plant Tested:	Test: 1 pm10	•	(as received basis)	
Boiler:	John Thompson Boiler **		21.0 %	
Firing system:	Perfect spreader.	= Ash ==================================		1 1
Emission control:	Multi Cyclone	Calorific Value	22.2 MJ/kg	
Average steam load:	8.5 Tn/Hr	Type	Rotowaro	
Measurement Standard:	USEPA Method 201A – Determination of PM10 Emissions (Constant Sampling Rate Procedure).	ions (Constant Sampling Rate Procedu	ıre).	
	USEPA Method 1 - Sample and velocity traverses for stationary sources.	tationary sources.	· •	
	USEPA Method 2 – Determination of stack gas velocity and volumetric flow rate (type S Pitot tube)	and volumetric flow rate (type S Pito	t tube)	
	USEPA Method 4 – Determination of moisture content in stack gases USEPA Method 4 – Determination of moisture content in stack gases USEPA Method 17 – Determination of Particulate Matter Emissions from Stationary Sources	or my morecular weight in stack gases er Emissions from Stationary Sources		
Conditions at Sampling Plane:	See figures 1 & 2	Stack diameter/Duct dimensions:	0.960 ш	
Conditions of Gas at Sample Point: * .	= * % Dry (vol.) . % Wet (mass) == *	Sampling start time: = *	arman 10:08	
Oxygen content:	8.0 8.3 %	Stack gas pressure:	102.12 kPa	
Carbon dioxide content *:	11.7 16.7 %	Average temperature:	J. 681	
Carbon monoxide content (ppm dry):	53 0.00 %	Stack gas density:	0.791 kg/m^3	
Nitrogen content #:	72.8 %	Average gas velocity:	8.261 m/s	
Gas moisture content:	3.7 2.2 %	Dry gas volumetric flow rate:	12,317 dsm³/hr	
Conditions of Sampling:		-		
Nozzle internal diameter:	7.61 mm	Sampling Method:	Cumulative sampling	
Isokinicity:	82.6 %	Suction nozzle type:	Sharp-edged stainless steel nozzle	
Sample time at each point:	4.89 min	Equipment arrangement:	Water removal upstream of the gas meter	
Total sample time:	60 min	Particulate drying:	Washing with Water, evaporating at clean ambient	
Gas meter reading start:	1551.961 m ³		condition, drying in oven 105°C.	
Gas meter reading stop:	1552.650 m³	Particulate separator:	Glass microfibre filter with size 47mm	
Gas meter static-pressure:	-0.08 kPa	Leakage tests performed by:	MA – SG	
Gas meter inlet temperature:	22 °C	Results:		
Dry gas volume sampled:	0.640 dsm ³	% of PM ₁₀ particulates:	% 09	
Particulate matter collected:	, 155.3 mg	Concentration of PM ₁₀ particulates @ 12.0% CO ₂ ;	149	mg/dsm ³
Notes	-			
* CO ₂ is calculated in accordance with M(1-O ₂ /20.9) where M is the theoreti	$(1-0_2/20.9)$ where M is the theoretical maximum CO ₂ content for	cal maximum CO_2 content for a given fuel when combusted with no excess air.	sess air.	7
# dry N volume by difference	•	All gas volumes are expressed at 273 K and 101.325 kPa.	. K and 101.325 kPa.	1
Allowable variation from isokinetic conditions is 80 to 120%	tions is 80 to 120%	$dsm^3 = dry standard cubic metre (273 K, 101.325 kPa)$		CRI Energy Ild

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	Date of Test: 73	27/3/11 Company:	Alico Walloa
Description of Plant Tested:	Test: 2	2 pm10 Fuel analysis:	(as received basis)
, , , , ,	ŧ		(crem marray on)
boller:			21.0 %
- Firing-system:	To Perfect spreader + First Street From Street	TAShTER ShT	
Emission control:	Multi Cyclone	Calorific Value	22.2 MJ/kg
Average steam load:	8.7 Tn/Hr	Type	Rotowaro
Measurement Standard:	USEPA Method 201A - Determination of PM10 Emissions (Constant Sampling Rate Procedure)	missions (Constant Sampling Rate Pr	
	USEPA Method 1 – Sample and velocity traverses for stationary sources.	for stationary sources.	
	USEPA Method 2 - Determination of stack gas velocity and volumetric flow rate (type S Pitot tube)	locity and volumetric flow rate (tyne S	Pitot tuhe)
	USEPA Method 3 - Gas Analysis for the determination of dry molecular weight	ation of dry molecular weight	
	USEPA Method 4 – Determination of moisture content in stack gases USEPA Method 17 – Determination of Particulate Matter Emissions from Stationary Sources	ntent in stack gases Matter Emissions from Stationary Son	ITOES
Conditions at Sampling Plane:	See figures 1 & 2	Stack diameter/Duct dimensions:	ions: 0.960 m
Conditions of Gas at Sample Point: :	: car = % Dry (vol.) % Wet (mass) =	- Sampling start time:	11:50
Oxygen content:	7.6 7.9 %	Stack gas pressure:	102.12 kPa
Carbon dioxide content *:	12.1 17.2 %	Average temperature:	188 °C
Carbon monoxide content (ppm dry):	37 0.00 %	Stack gas density:	0.794 kg/m ³
Nitrogen content #:	80.3	Average gas velocity:	
Gas moisture content:		Dry gas volumetric flow rate:	11.730
Conditions of Sampling:			
Nozzle internal diameter:	7.605 mm	Sampling Method:	Cumulative sampling
Isokinicity:	87.6 %	Suction nozzle type:	Sharp-edged stainless steel nozzle
Sample time at each point:	5.07 min	Equipment arrangement:	Water removal upstream of the gas meter
Total sample time:	60 min	Particulate drying:	Washing with Water, evaporating at clean ambient
Gas meter reading start:	1552.663 m ³		condition, drying in oven 105°C.
Gas meter reading stop:	1553.361 m ³	Particulate separator:	Glass microfibre filter with size 47mm
Gas meter static-pressure:	-0.08 kPa	Leakage tests performed by:	MA - SG
Gas meter inlet temperature:	23 °C	Results:	
Dry gas volume sampled:	0.645 dsm ³	% of PM ₁₀ particulates:	% 08
Particulate matter collected:	124.4 mg	. Concentration of PM ₁₀ particulates @ 12.0% CO ₂ :	ticulates @ 12.0% CO ₂ : 155 mg/dsm ³
. Notes:			
* CO ₂ is calculated in accordance with M(1	* CO ₂ is calculated in accordance with M(1-O ₂ /20.9) where M is the theoretical maximum CO ₂ content for a given fuel when combusted with no excess air.	for a given fuel when combusted with no	excess air.
# dry N volume by difference		All gas volumes are expressed at 273 K and 101.325 kPa	1 273 K and 101.325 kPa
		•	

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Posteription of Plant Tested: John Thompson Boiler Pacific Spreader* Pacific S	Puel analysis: Moisture ———————————————————————————————————
Boiler: Firing system: Firing system: Average steam load: Multi Cyclone Average steam load: Multi Cyclone Average steam load: Multi Cyclone Average steam load: B. O TuHr Measurement Standard: USEPA Method 2 — Determination of PM10 Emissions (USEPA Method 2 — Determination of Stack gas velocity and USEPA Method 3 — Gas Analysis for the determination of USEPA Method 4 — Determination of Particulate Matter En USEPA Method 4 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 2 — See figures 1 & 2 Conditions of Gas at Sample Point: Carbon dioxide content (ppm dry): Nitrogen content (ppm dry): Nozele internal diameter: See figures 1 & 2 Sample time at each point: Gas meter reading start: Gas meter reading stop: 1533.333 m³ Gas meter reading stop: 1533.333 m³ Gas meter reading stop: 1540 min Gas meter reading stop: 1554.082 m³ Gas meter reading stop: 1564.8 dsm³ Gas meter reading stop: 157 % Gas meter reading stop: 158.3 % Gas meter reading stop: 159 % 169 % 170	21.0 % 22.2 MJ/kg 22.2 MJ/kg 4.6 % 12.2 MJ/kg 0.960 m 0.960 m 17.9 °C 0.811 kg/m³ 6.088 m/s 9,261 dsm³/hr ulative sampling
Emission control: Average steam load: Multi Cyclone Average steam load: Built Cyclone Average steam load: Built Cyclone Average steam load: Built Cyclone Built Cy	4.6 % 22.2 MJ/kg towaro 0.960 m 0.960 m 102.13 kPa 179 °C 0.811 kg/m³ 6.088 m/s 9,261 dsm³/hr ulative sampling
## Multi Cyclone ## Outside Cyclone ## Outside Cyclone ## USEPA Method 201A — Determination of PM10 Emissions (USEPA Method 1 – Sample and velocity traverses for station USEPA Method 2 – Determination of stack gas velocity and USEPA Method 3 – Gas Analysis for the determination of USEPA Method 4 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En Welpa Method 17 – Determination of Particulate Matter En ## Outside Control of Control of Control of Control of Particulate Matter En ## Outside Particulate Particul	Emissions (Constant Sampling Rate Procedure). Soft stationary sources. Soft stationary sources. Slack gases Matter Emissions from Stationary Sources Stack diameter/Duct dimensions: 0.960 m Stack gas pressure: 102.13 kPa Average temperature: 179 °C Stack gas density: 0.811 kg/m³ Average gas velocity: 6.088 m/s Dry gas volumetric flow rate: 9,261 dsm³/hr Sampling Method: Cumulative sampling
## S.0 Tn/Hr USEPA Method 201A – Determination of PM10 Emissions (USEPA Method 2 – Determination of PM10 Emissions (USEPA Method 2 – Determination of stack gas velocity and USEPA Method 3 – Gas Analysis for the determination of dr USEPA Method 4 – Determination of moisture content in sta USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En 12.9 #:	Emissions (Constant Sampling Rate Procedure). Sofor stationary sources. Slocity and volumetric flow rate (type S Pitot tube) antion of dry molecular weight ment in stack gases Matter Emissions from Stationary Sources Matter Emissions from Stationary Sources Stack diameter/Duct dimensions: 0.960 m Stack diameter/Duct dimensions: 0.960 m Stack gas pressure: 102.13 kPa Average temperature: 179 °C Stack gas density: 0.811 kg/m³ Average gas velocity: 6.088 m/s Dry gas volumetric flow rate: 9,261 dsm³/hr Sampling Method: Cumulative sampling
USEPA Method 201A - Determination of PM10 Emissions (USEPA Method 1 - Sample and velocity traverses for station USEPA Method 2 - Determination of stack gas velocity and USEPA Method 3 - Gas Analysis for the determination of dr USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Matter En USEPA Method 17 - Determination of Particulate Method 17 - Determination of Particulate Method 18 desm² and Particulate En USEPA Method 17 - Determination of Particulate En USEPA Method 18 - Determination of Particulate En USEPA Method 17 - Determination	Emissions (Constant Sampling Rate Procedure). s for stationary sources. elocity and volumetric flow rate (type S Pitot tube) nation of dry molecular weight mater in stack gases Matter Emissions from Stationary Sources Stack diameter/Duct dimensions: 0.960 m Stack gas pressure: 0.960 m Stack gas pressure: 102.13 kPa Average temperature: 179 °C Stack gas density: 0.811 kg/m³ Average gas velocity: 6.088 m/s Dry gas volumetric flow rate: 9,261 dsm³/hr Sampling Method: Cumulative sampling
USEPA Method 1 – Sample and velocity traverses for station USEPA Method 2 – Determination of stack gas velocity and USEPA Method 3 – Gas Analysis for the determination of dr USEPA Method 4 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En USEPA Method 17 – Determination of Particulate Matter En 8.7	s for stationary sources. slocity and volumetric flow rate (type S Pitot tube) aution of dry molecular weight antion of dry molecular weight ment in stack gases Matter Emissions from Stationary Sources Stack diameter/Duct dimensions: 0.960 m Stack gas pressure: 102.13 kPa Average temperature: 102.13 kPa Average temperature: 102.13 kPa Average gas velocity: 6.088 m/s Dry gas volumetric flow rate: 9,261 dsm³/hr Sampling Method: Cumulative sampling
USEPA Method 2 — Determination of stack gas velocity and USEPA Method 3 — Gas Analysis for the determination of dr USEPA Method 4 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 80.4 72.6 % 3.7 2.2 % 3.7 2.2 % 3.7 2.2 % 3.7 2.2 % 3.7 2.2 % 4.93 min 60 min 1553.383 m³ 1554.082 m³ 1554.082 m³ 1554.082 m³ 1554.082 m³ cted: 103.9 mg	shocity and volumetric flow rate (type S Pitot tube) nation of dry molecular weight nnent in stack gases Matter Emissions from Stationary Sources Stack diameter/Duct dimensions: 0.960 m Stack gas pressure: 102.13 kPa Average temperature: 179 °C Stack gas density: 6.088 m/s Dry gas volumetric flow rate: 9,261 dsm³/hr Sampling Method: Cumulative sampling
USEPA Method 4 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En USEPA Method 17 — Determination of Particulate Matter En Website 12 & Wet (mass) = " ·	
## See figures 1 & 2 mple Point:	Stack diameter/Duct dimensions: Sampling start time: Stack gas pressure: Average temperature: Stack gas density: Average gas velocity: Dry gas volumetric flow rate: Sampling Method:
#: 12.9 % Wet (mass) " " " 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.9 % 6.7 6.7 6.9 % 6.7 6.7 6.9 % 6.7 6.7 6.7 6.7 6.7 6.7 6.7 6.7 6.7 6.7	Sampling start time: "Stack gas pressure: Average temperature: Stack gas density: Average gas velocity: Dry gas volumetric flow rate: Sampling Method:
*; 12.9 6.7 6.9 % *t: 12.9 18.3 % *t: 21 0.00 % 80.4 72.6 % 3.7 2.2 % *t: 87 mm ' 85.1 % int: 60 min 1553.383 m³ 1554.082 m³ tre: -0.07 kPa d: 0.648 dsm³ cted: 103.9 mg	s: // flow rate:
*: 12.9 18.3 % snt (ppm dry): 21 0.00 % 80.4 72.6 % 3.7 2.2 % 3.7 2.2 % sr: 8.7 mm ' 85.1 % int: 60 min 1553.383 m³ 1554.082 m³ ture: 23 °C d: 0.648 dsm³ cted: 103.9 mg	S. A.
nt (ppm dry): 21 0.00 % 80.4 72.6 % 3.7 2.2 % 3.7 2.2 % ar: 8.7 mm 85.1 % int: 4.93 min 60 min 1553.383 m³ 1554.082 m³ tee: -0.07 kPa 4: 0.648 dsm³ cted: 103.9 mg	/; flow rate:
80.4 72.6 % 3.7 2.2 % 3.7 2.2 % ar: 8.7 mm 85.1 % 14.93 min 60 min 1553.383 m³ 1554.082 m³ 1554.082 m³ 103.9 mg Relation (103.9 mg) 103.9 mg	flow rate:
3.7 2.2 % ar: 8.7 mm 8.1 mm 85.1 % int: 4.93 min 60 min 1553.383 m³ 1554.082 m³ 1554.082 m³ 23 °C 43	flow rate:
rr: 8.7 mm ' 85.1 % 85.1 % int: 4.93 min 60 min 1553.383 m³ 1554.082 m³ 1554.082 m³ 23 °C d: 0.648 dsm³ cted: 103.9 mg	
le internal diameter: 1. 1. 2. mm 1. 2. min 1. 2. min 1. 2. min 2. min 2. min 3. min 4.93 min 4.93 min 60 min 60 min 60 min 61 meter reading start: 60 1. min 61 min 62 min 63 min 64 min 654.082 m ³ 66 min 67 meter reading start: 67 meter reading stop: 68 min 69 min 60	
10 10 10 10 10 10 10 10	
le time at each point: 1 sample time: 1 samp	Suction nozzle type: Sharp-edged stainless steel nozzle
t sample time: meter reading start: meter reading stop: meter static-pressure: -0.07 kPa meter static-pressure: 23 °C gas volume sampled: culate matter collected: 103.9 mg	Equipment arrangement: Water removal upstream of the gas meter
meter reading start: 1553.383 m³ meter reading stop: 1554.082 m³ meter static-pressure: -0.07 kPa meter inlet temperature: 23 °C gas volume sampled: 0.648 dsm³ culate matter collected: 103.9 mg	Particulate drying: Washing with Water, evaporating at clean ambient
meter reading stop: meter static-pressure: -0.07 kPa meter inlet temperature: gas volume sampled: 0.648 dsm³ culate matter collected: 103.9 mg	condition, drying in oven 105°C.
meter static-pressure: -0.07 kPa meter inlet temperature: 23 °C gas volume sampled: 0.648 dsm³ culate matter collected: 103.9 mg	Particulate separator: Glass microfibre filter with size 47mm
meter inlet temperature: 23 °C gas volume sampled: 0.648 dsm³ culate matter collected: 103.9 mg	Leakage tests performed by: MA - SG
gas volume sampled: 0.648 dsm³ culate matter collected: 103.9 mg	Results:
culate matter collected: 103.9 mg	% of PM10 particulates:
Notes	Concentration of PM ₁₀ particulates @ 12.0% CO ₂ : 135 mg/dsm ³
10163	
* CO ₂ is calculated in accordance with M(1-O ₂ /20.9) where M is the theoretical maximum CO ₂ content for a given fuel when combusted with no excess air	tent for a given fuel when combusted with no excess air
# dry N volume by difference	All gas volumes are expressed at 273 K and 101.325 kPa.
Allowable variation from isokinetic conditions is 80 to 120%	dsm ³ = dry standard cubic metre (273 K, 101.325 kPa)

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Summary Table

<u> </u>	Test 1	Test 2	Test 3	Average	Units
Actual Concentration of total particulate at 12% CO ₂ :	250	192	150	197	mg/dsm ³
Concentration of PM ₁₀ particulates at 12% CO ₂ :	149	155	135	146	mg/dsm ³
PM₁0 %:	59.7	80.5	90.4	77	%

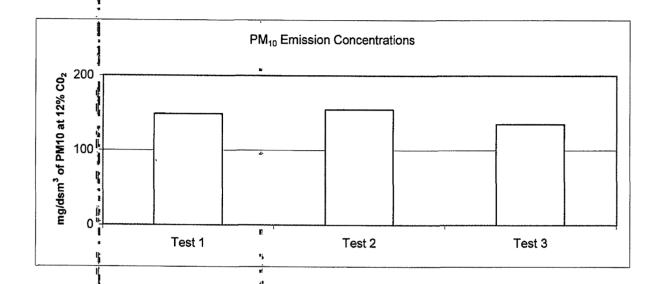


Figure 2: Sampling plane.

Shape Circular
Approximate diameters upstream from interferences (after sampling point) ~9.0 Approximate diameters downstream from Interferences (before sampling point) ~6 Approximate dameters downstream from interferences (before sampling point complies with the test method requirements, inside diameter (iD) of stack (m) 1

Stack onentation Vertical

Angle of gas flow Laminar

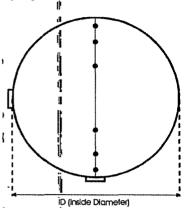
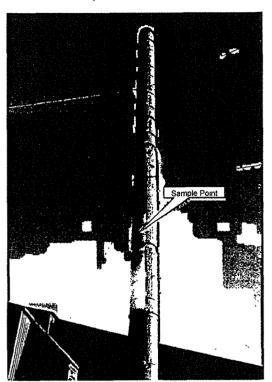


Figure 1: Sampling location

Stack has been changed but similar to old stack



		SIONS TEST	SHEEL					Test:	1 pm10
CRL Ref:	11-	31304	Site:	: Affco Wairoa					
raverse point	Time (min)	Sample point position (m)	Velocity pressure	Rota-meter setting (Vmin)	DGM temp	Stack temp (*C)	O ₂ (%)	CO (ppm)	VAC (kPa)
1	4.71	0.042	0.13	11.58	20.7	188.8	8:2	40'	-46
2	9.60	0.140	0.14	11.58	21,1	188.3	8'8'	52	-54
3	14 83	0.284	0.16	11.58	21:.9	188.6	7.5	55	-60
4	20.05	0.676	0.16	11.58	22.3	188.3	8:4	59	-66
5	25.11	0.820	0.15	11.58	22.5	189.1	7.6 [,]	58	-70
6	30.00	0.918	0.14	11.58	22.6	189.3·	77	56	-76
7	34.71	0:042	0 1/3	11.58	23.1	188.9 ⁻	8.0	53	-82'
8	39.60	ଡୁ:140	0:.14'	11.58	23.4	189:3.	7.3	53	-86·
9	44.83	0.284	0.16	11.58	23.4	189:1	7.8	53	-88
10	50.05	0.676	0.16	11.58	23:3	188.7	8.1	50⊦	-96
11	55.11	0.820	0.15	11.58	23.4	188.7	7.8	46	-100
12	60.00	0.918	0.14	11.58	23:7	190.0	7.8	44	-100
		0.010		11.00		1			
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VERAGE	s ·		0.1467	11.58	21.85	188.73	8.03	53.33	-62.00
as Meter Si	ART (1551.961		Test Time	(min)		60	
i i					No. Traverse	Points		12	
s Meter ½ Way			n/a '		Static	("WG)		-0.31	
Sas Motor Si	OP #	1552.650		Nozzie o	(mm)		7.61		
Sas Meter Fa	ictor ij	0.995		Stack é (m)		0.960			
eakage Tes	- 4	0.995 MA – SG		 	Duct (m)		d x w		
		0.86			11-A27		Mass (g) 0.1077		
Plant Descrip	n d	John Thomps	n Bailer		Filter No.		11-A27 mass (g)		
······································	- 1	ļ	John Thompson Boiler		Fulsales Control		Billiti Cyalana		
iring System		Perfect spreader			Emission Control		Multi Cyclone		etop.
verage Stea	in road i	8.5 Tn/Hr		Impingers		START		STOP	
	ļ	Date	ļ	3/11	No 1 (g)	501.			503
	1	Start Time	<u> </u>	a.m.	No 2 (g)	469		<u> </u>	182.3
		End Time	11:08	a.m.	No 3 (g)	393.			396
		Balance Check (, 	B .	Silica (g)	813		ļ	315.7
OL ENG		Moisture %	21	Ash %	4.6	CV (MJ/kg)	22.24	Туре	Rotowar
		Assu	med Duct Moistu	re %	7	Atmospheric Pro		↓	02.20
		l eaker	je Test	* Pre St	art/Stop	1551.9	9606	15	1.9606
CRL Ene	rgy Lid	Leana	y www.	Post St	art/Stop	1552.6	512	159	52.6512 .

		SSIONS TEST						Test:	2 pm10
CRL Ref: 11-31304 Site:		Site:	Affco Wairoa						
raverse point	Time	Sample point position	Velocity pressure	Rota-meter setting	DGM temp	Stack temp	O ₂	со	VAC
ì	(min)	(m)	("WG) .	(Vmin)	(°C)	(°C)	(%)	(ppm)	(kPa)
1	5.07	0:042	0:14	11.76	23.8	188.0	8.0	38	-46
2	10.13	, 0.140₁	, 0.14	11.76	23:7	188.1	79	38	-52
3	15.55	0.284	0.16	11.76	23:4	188.0	7.3'	38.	-62
4	20.43	0.676	0.13	11.76	23:2	188.2	7.2	37	-68
5	25.13	0.820	0.12	11.76	23.21	187.9	7.7	37	-74
6	29.62	0.918	0.11	11.76	22:9'	187.9	7.7	35	-78
7	34:31	0.042	0.12	11.76	22:7	187.6	8:0	32	-84
8	39:55	0 1'40	0.15	11.76	22:8	187.5	7.7	31	-86
9	44.62	0:284	0.14	11.76	22.6	188.0'	7.2	29	-94
10	49.69	01676	0.14	11.76	22.6	188:01	7.3	27	-98
11	54.93	0:820	0.14	11.76	22.7	187.6	8.1	28	-100
12	60.00	0.918	0.15	11.76	22.7	186.2	6.3	23	-100
-12	60.00	0.916	U-14	11./6	22.9	180.2	0.0	23 1	-100
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VERAGE	s		0.1333	11.76	23.37	188.02	7.63	37.17	-63.33
as Meter S			1552.663		Test Time	(min)		60	
	#				No. Traverse Points		12		
s Meter ½	Way :		n/a	n/a		Static ("WG)			
			1553.361		Nozzie è	(mm)		7.61	
Gas Meter STOP 1 1 Gas Meter Factor 1		0.995		- 			0.960		
					Stack ø	(m)			
Leakage Test By:		MA - SG		Duct	(m)		d x w		
itot Consta			0.86		Filter No.		11-A29	Mass (g)	0.1075
lant Descri	<u> </u>	John Thomp	son Boiler		·				
ring Syster	m	Perfect spre	ader	Emission Co		ntrol Multi Cyc		olone .	
Average Steam Load		8.7 Tn/Hr			Impingers	START		STOP	
	1	Date	29/	3/11	No 1 (g)	503.	0		505
	,	Start Time	11:50) a.m.	No 2 (g)	482.	3	4	195.4
		End Time	12:51	l p.m.	No. 3 (g)	396			398.6
<i></i>		Balance Check	(+/-)		Silica (g)	815.	7		317.9
Moisture %		Moisture %	21	Ash %	4.6	CV (MJ/kg)	22.24	Туре	Rotoward
		med Duct Moistu	<u> </u>	7	Atmospheric Pre			02.20	
		1		Pre Start/Sto				1552.6630	
7	!		ige Test			 		 	2.6630

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PARŢICU	LATE EMIS	SIONS TEST	SHEET					Test:	3 pm10	
CRL Ref:	, 11-	-31304	Site:	Affco Wairoa						
raverse point	Tune (min)	Sample point position (m)	Velocity pressure	Rota-meter setting (Vmin)	DGM temp (*C)	Stack temp (*C)	O ₂ (%)	CO (ppm)	VAC (kPa)	
1	4.93	0.042	0:08	11.76	22.9	180.2	7.4	21	-48	
2	9:85	0.140	0.08	11.76	22.9	180.1	7.2	25	-54'	
3	15.08	0.284	0.09	11.76	22:6	178.0	7.5 [,]	25	-64	
4	20.31	0,676	0.09	11.76	22:5	178.7	5.5	22	-70	
5	25.23	0.820	0.08	11.76	22:6	179.6	6:6	19	-78	
6	29.84	0.918	0,07	11.76	22.6	1'80'.2'	6:0 [,]	16	-84	
Ż	34.77	0:042	0.08	11.76	22.8	179.9	6.2	17	-88	
8	39.69	0:140	0:08	11.76	22.7	17943	7.3	16	-92	
9	44 92	0:284	0,09	11.76	22.6	178.4	7.0	16	-96·	
10	50.15	0.676	0,08	11.76	22.7	177.8	6.9	15	-98	
11	55.07	0.820	0:08	11.76	22.7	177.8	6.9	14	-100	
12	60.00	0.918	0.08	11.76	22.7	177.5	6.4	1'4	-100	
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			<u> </u>							
VERAGE	s !		0.0817	11.76	22.68	179.47	6 70	21.33.	-66.33	
Sas Meter S			1553.383	<u> </u>	Test Time	(min)		60		
ı	1			No. Traverse	No. Traverse Points		12 .			
s Meter ½			n/a	n/a r		Static ("WG)		-0.30		
Sas Meter STOP 1554.082			Nozzle		8.7					
as Meter Fa	44		0.995	Stack ø		(m)	(m) 0.960		****	
.eakage Tes	kage Test By: MA - SG			Duct	(m)		dxw			
Pitot Consta	nt]		0.86		Filter No.		11-A28	Mass (g)	0.1063	
lant Descri	ption	John Thomp	son Boiler					.	-	
iring Syster	n 1	Perfect sprea	ader		Emission Co	ontrol	Multi Cyc	lone		
verage Stea	m Load	8.0 Tn/Hr			Impingers	START		STOP		
E .		Date 29/3/11		No 1 (g)	505		507.0			
		Start Time			No. 2 (g)	495.4		ļ	508.5	
		End Time			No 3 (g)	ļ			401.2	
		Balance Check		<u>.</u> -	Silica (g)	<u> </u>	817.9		820.1	
	1 1	Moisture %	21	Ash %	4.6	CV (MJ/kg)	22.24	Туре	Rotowar	
Q	N. A. S.		med Duct Moistu		7	Atmospheric Pro			02.20	
					art/Stop	1553.3			53.3828	
CDI F		Leakage Test		· · · · · · · · · · · · · · · · · · ·	 					

1554.1118

1554.1118

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John Thompson Boiler

CRL Report No:

#11-31304
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Leak Test: Carried out before and after each test by creating a vacuum of 60 Kpa within the sampling train. A drop in vacuum pressure indicates a leak. Bubbles are also seen in the impingers. If the

Test 1

Particulate Matter Collected		
Filter start weight	0 1077	g
Beaker start weight	1.3094	g
Filter & beaker stop weight	1.5016	g
Filter Gain 1	0.0845	g
wash pm10 (beaker)	110.5408	g
wash pm10 (beaker with residue)	110.5490	g
pm10 wash Gāin	0.0082	g
Nozzle and fittings (Total) wash (beaker)	123.1096	g
Nozzle and fittings (Total) wash (beaker with residue)	123.1795	g
Particulate matter collected F	0.0228	g
Nozzle and fittings blank (beaker)	99.3950	g
Nozzle and fittings blank (beaker with residue)	99.4023	g
Blank Gain	0.0073	g

Particulate Matter Collected

Filter start weight	0.1075	g
Beaker start weight	1.3053	g
Filter & beaker stop weight	1.5001	g
Filter Gain	0.0873	, g
wash pm10 (beaker)	94.2561	' g
wash pm10 (beaker with residue)	94.2689	g
pm10 wash Gain	0.0128	g
Nozzle and fittings (Total) wash (beaker)	111 9787	g
Nozzle and fittings (Total) wash (beaker with residue)	112.0103	g
Particulate matter collected	0.0685	g
Nozzle and fittings blank (beaker)	99 3950	g
Nozzle and fittings blank (beaker with residue)	99.4023	g
Blank Gain	0 0073	g

Test 3

Test 2

Particulate Matter Collected		
Filter start weight	0.1063	g
Beaker start weight	1.2979	g
Filter & beaker stop weight	1.4891	g
Filter Gain	0.0849	g
wash pm10 (beaker)	121.5746	g
wash pm10 (beaker with residue)	121.5836	g
pm10 wash Gain	0.0090	g
Nozzle and fittings (Total) wash (beaker)	106.0558	g
Nozzle and fittings (Total) wash (beaker with residue)	106.0731	g
Particulate matter collected	0.0766	g
Nozzle and fittings blank (beaker)	99.3950	g
Nozzle and fittings blank (beaker with residue)	99.4023	g
Blank Gain	0.0073	g